



MANICALAND STATE UNIVERSITY OF APPLIED SCIENCES

FACULTY OF ENGINEERING, SCIENCE AND TECHNOLOGY

DEPARTMENT: CHEMICAL AND PROCESSING ENGINEERING

MODULE: FLUID SOLID SYSTEMS

CODE: CHEP 313

SESSIONAL EXAMINATIONS

JUNE 2023

DURATION: 3 HOURS

EXAMINER: MRS C. MUHEZWA

INSTRUCTIONS

- 1. Answer **All** questions.*
- 2. Start a new question on a fresh page*
- 3. Total marks 100*

Additional material(s): Graph paper, Calculator

QUESTION 1

- a. Define the term *particle characterisation*. [3]
- b. Explain the meaning of the following terms as they are used in particle technology:
- Surface diameter*,
 - Surface-to-volume diameter*,
 - Martin's diameter*,
 - Feret's diameter*. [4x1]
- c. A solid sample from an industrial plant has cubic particles with average edge length of 3.2 μm . Determine the
- volume-equivalent sphere diameter (D_{volume}) [3]
 - surface-equivalent sphere diameter (D_{surface}) [3]
 - volume-surface equivalent sphere diameter (D_{sv}) of the particles [2]
- d. i. State the forces that act on a particle that is falling in a liquid. [3]
- ii. Hence derive the equation, of the terminal falling velocity of a particle of density ρ_p in a fluid of density ρ_f and viscosity μ . Assume the particle's motion is under gravity, in equilibrium, and is in the Stoke's region. [7]

QUESTION 2

- a. Explain the following
- dense phase pneumatic conveying* [3]
 - saltation velocity* [2]
 - choking velocity* [2]
- b. State **four** examples of particulate solids that can be transported by pneumatic conveying. [4]

- c. The general relationship between gas velocity and pressure gradient $\Delta P/\Delta L$ for a horizontal transport line is shown in Fig 1. Line AB represents the curve obtained for gas only in the line, CDEF for a solids flux, G_1 , and curve GH for a higher solids feed rate, G_2 .

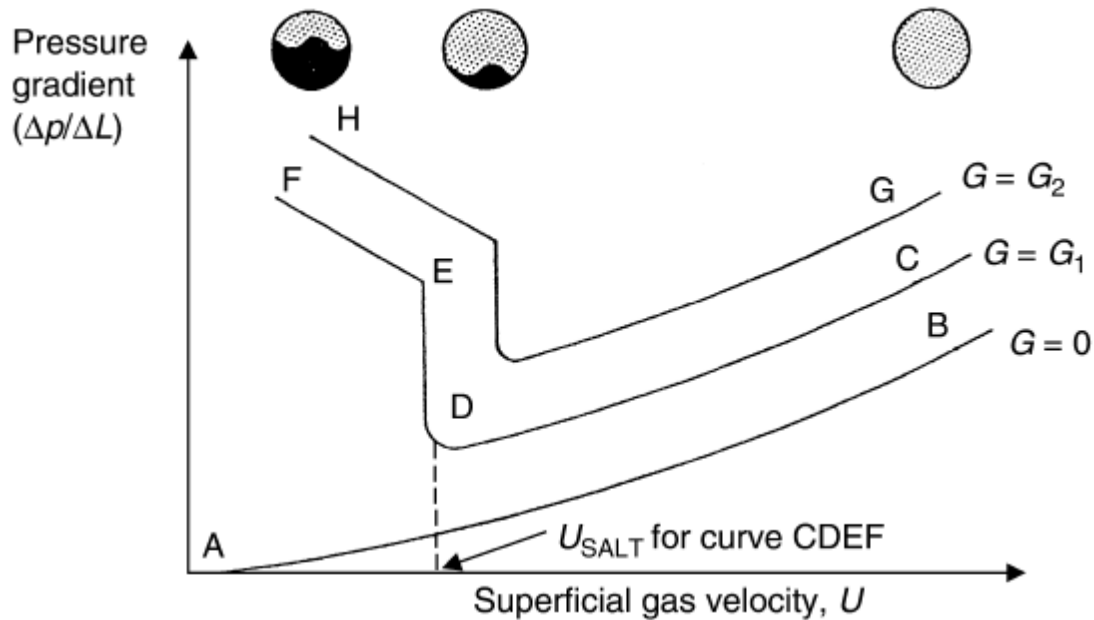


Fig. 1: Phase diagram for dilute phase horizontal pneumatic transport

- i. Describe and explain what happens if the gas velocity is reduced whilst solids feed rate is kept constant at G_1 [8]
 - ii. Explain the shape of the graph when $G = 0$ [3]
- d. What are the advantages of pneumatic conveying over mechanical conveying in particulate technology? [3]

QUESTION 3

- a. Describe the principle behind the *elutriation* method of particle size measurement. [5]
- b. What are the assumptions made in the sedimentation method of particle size measurement? [3]
- c. Crystalline fertiliser solid particles are immersed in a liquid solvent of viscosity 10 Pa s, and density 40 kg/m³. The density of the solid particles is 53 kg/m³ and their final settling velocity 5.3 m/s.
- What is meant by the '*final settling velocity*' [2]
 - Determine the equivalent Stokes diameter (D_s) of the fertiliser particles? Assume Stoke's law apply. [3]
- d. Explain the need for particle size reduction in particulate technology [2]
- e. State Rittinger's law of the energy needed for particle size reduction [2]
- f. A material is crushed in a Blake jaw crusher such that the average size of particle is reduced from 40 mm to 10 mm with the consumption of energy of 13.0 kW/(kg/s). What would be the consumption of energy needed to crush the same material of average size 85 mm to an average size of 15 mm:
- Assuming Rittinger's law applies? [3]
 - Assuming Kick's law applies? [3]
- g. What are the factors that affect the choice of machine selected for a particular grinding operation? [2]

QUESTION 4

- a. Describe the procedure necessary to choose the right sampling method in powder technology (sampling workflow) [6]
- b. Explain what is meant by *in situ* sampling [2]
- c. What are the advantages of *in situ* sampling? [3]
- d. Describe the principle behind the *coning and quartering* method of sampling [4]

- e. Describe the following methods of particle size enlargement as they are used in particle technology
 - i. Agglomeration [4]
 - ii. Fluidized beds [4]
- f. Differentiate between *differential* and *cumulative* particle size distributions [2]

END OF EXAMINATIONS