

**MANICALAND STATE UNIVERSITY OF APPLIED SCIENCES**

**FACULTY OF ENGINEERING**

**Chemical and Processing Engineering Department**

**CHEMICAL ENGINEERING THERMODYNAMICS II**

**CODE: HCHE 214**

**SESSIONAL EXAMINATIONS**

**APRIL 2021**

**DURATION: 3 HOURS**

**EXAMINER: K. NYENYAYI (MR)**

**INSTRUCTIONS**

1. Answer *any four questions*.
2. Each question carries 25 marks.
3. Total marks 100.

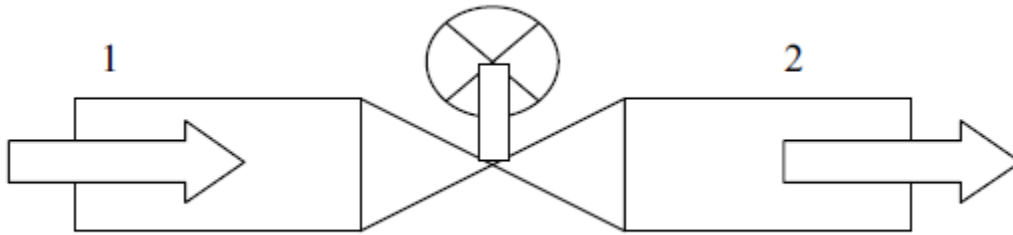
**ADDITIONAL MATERIALS**

Calculators, Steam tables.

This question paper consists of 5 printed pages

## QUESTION ONE

- a) With aid of P - V diagrams, define terms *cyclic process*, *heat engine* and *heat pump*. [7]
- b) Determine using Steam tables, the volume occupied by 2 kg of steam at 500 kPa, under the following conditions and specify the state of the steam.
- Pure liquid state.
  - When it is a pure vapour state.
  - 20% moisture content.
  - 20% dry
- [8]
- c) Consider flow of fluid through a small valve as shown;



- Describe *throttling process*. [3]
- Applying Steady Flow Energy Equation (SFEE) below
$$Q - W = (\Delta H + \Delta KE + \Delta PE)$$
and making necessary assumptions, show that for the control valve above, the enthalpy of the fluid remains constant. [7]

## QUESTION TWO

- a) With the aid of a clearly labelled block diagram and P-V or T-S diagrams, describe the process of steam production in chemical industry. Your description

should include the following aspects:

- The ideal Carnot cycle
- Impracticalities of the Carnot cycle
- The ideal Rankine cycle [20]

**b)** Calculate efficiency of Carnot cycle for a system with hot reservoir temperature ( $T_h$ ) of 500 K and cold reservoir temperature ( $T_c$ ) of 350 K. [5]

### QUESTION THREE

**a)** A steam turbine operates adiabatically at a power level of 3500 kW. Steam enters the turbine at 3000 kPa and 773.15 K and exhausts the turbine at as saturated vapour at 20 kPa.

- i. What is the steam rate through the turbine?
- ii. What is the turbine efficiency? [10]

**b)** An adiabatic compressor has been designed to continuously compress 1kg/s of saturated vapour steam from 100 kPa to 10 000 kPa and 1100 °C.

- i. Estimate the power requirement of this compressor in kW.
- ii. Determine the efficiency of the compressor. [10]

**c)** Using examples, distinguish between *internal* and *external combustion engines*. [5]

### QUESTION FOUR

**a)** What is Theoretical Flame Temperature (TFT) ? [2]

**b)** Define the terms Gross Calorific Value (GCV) and Net (lower) Calorific Value (NCV). Give a mathematical relationship between the two. [5]

**c)** A medium sized boiler has the following specifications. Determine the boiler efficiency based on the net calorific value of the fuel.

- Steam output  $31.6 \text{ kgs}^{-1}$
- Steam pressure 6 MPa
- Steam temperature  $500^\circ\text{C}$
- Boiler Feed Water (BFW) temperature  $100^\circ\text{C}$
- Fuel (Nat. Gas) -96.5 v/v%  $\text{CH}_4$ , 0.5v/v%  $\text{C}_2\text{H}_6$ , remainder non-combustible
- GCV =  $38,700 \text{ kJm}^{-3}$  at  $25^\circ\text{C}$
- Fuel consumption  $2.9 \text{ m}^3\text{s}^{-1}$

$$\text{Boilerefficiency } (\eta) = \frac{\text{Energy Output to water}}{\text{Energy Input from fuel}} \quad [18]$$

### QUESTION FIVE

- a) Describe liquefaction process and outline how the process can be achieved. [5]
- b) With aid of diagram, outline the Linde Liquefaction process. [17]
- c) Give any 3 industrial applications of liquefaction process. [3]

Process	Constant Volume	Constant Pressure	Constant Temperature	Polytropic	Reversible Adiabatic or Isentropic
Law	$\frac{P}{T} = \text{const}$	$\frac{V}{T} = \text{const}$	$PV = \text{const}$	$PV^n = \text{const}$	$PV^\gamma = \text{const}$
P, V, T, Relation	$\frac{P_1}{T_1} = \frac{P_2}{T_2}$	$\frac{V_1}{T_1} = \frac{V_2}{T_2}$	$P_1V_1 = P_2V_2$	$P_1V_1^n = P_2V_2^n$ $\frac{P_1}{P_2} = \left(\frac{V_2}{V_1}\right)^n$ $= \left(\frac{T_1}{T_2}\right)^{\frac{n}{n-1}}$	$P_1V_1^\gamma = P_2V_2^\gamma$ $\frac{P_1}{P_2} = \left[\frac{V_2}{V_1}\right]^\gamma$ $= \left[\frac{T_1}{T_2}\right]^{\frac{\gamma}{\gamma-1}}$
Change in Internal Energy $\Delta U$	$mC_v(T_2 - T_1)$	$mC_v(T_2 - T_1)$	0	$mC_v(T_2 - T_1)$	$mC_v(T_2 - T_1)$
Work Transfer $W = \int p dv$	0	$P(V_2 - V_1)$ Or $mR(T_2 - T_1)$	$PV \ln \frac{V_2}{V_1}$ Or $mRT \ln \frac{V_2}{V_1}$	$\frac{P_1V_1 - P_2V_2}{(n-1)}$  $\frac{mR(T_1 - T_2)}{(n-1)}$	$\frac{P_1V_1 - P_2V_2}{(\gamma-1)}$  $\frac{mR(T_1 - T_2)}{(\gamma-1)}$  $mC_v(T_1 - T_2)$
Heat Transfer Q	$mC_v(T_1 - T_2)$	$mC_p(T_1 - T_2)$	$PV \ln \frac{V_2}{V_1}$ Or $mRT \ln \frac{V_2}{V_1}$	$W + (U_2 - U_1)$	0
Change in Entropy $\Delta S = S_2 - S_1$	$mC_v \ln \frac{T_2}{T_1}$ or $mC_v \ln \frac{P_2}{P_1}$	$mC_p \ln \frac{T_2}{T_1}$ or $mC_p \ln \frac{V_2}{V_1}$	$mR \ln \frac{V_2}{V_1}$ or $mR \ln \frac{P_1}{P_2}$	$m \left[ R \ln \frac{V_2}{V_1} + C_v \ln \frac{T_2}{T_1} \right]$  $m \left[ R \ln \frac{P_1}{P_2} + C_p \ln \frac{T_2}{T_1} \right]$  $m \left[ C_p \ln \frac{V_2}{V_1} + C_v \ln \frac{P_2}{P_1} \right]$	0

Table 1: List of Perfect Gas Relations